

Progress Report Meeting

May 22, 2012

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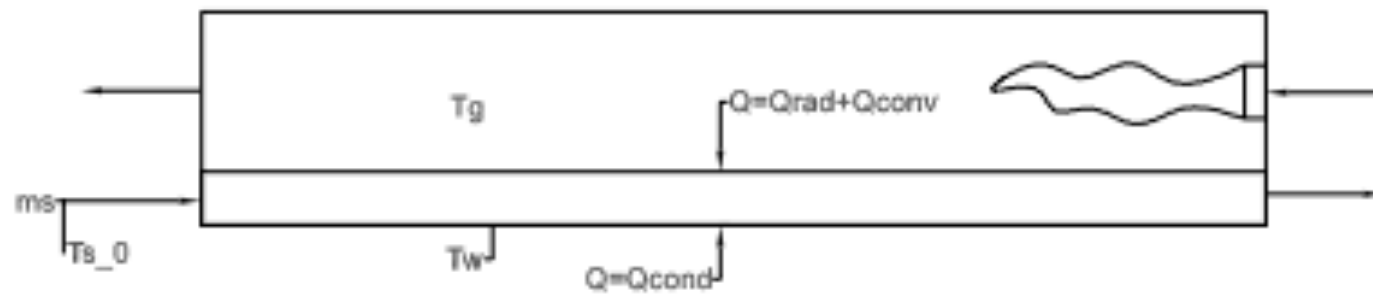


1-D PFR Model (ODE)

Why use a simplified model?

- It may give good results due to the low loading of the kiln
- It can be used as an aid for decisions in the re-design of the operation unit, e.g. the temperature of the feed can be changed easily and the computation time is seconds (to evaluate preheating of the feed for example)
- It will be used for an initial solution for further models

1-D/2-D Sketch of the Kiln



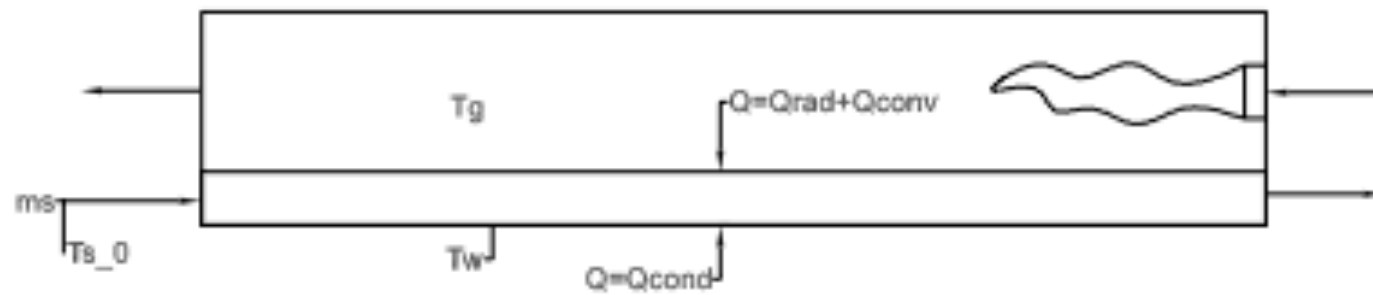


Assumptions of the Model

- The freeboard gases are homogeneously mixed in the transversal direction,
- The granular material is perfectly mixed in the transversal direction,
- The granular material flows in a PFR-like manner.

One must note that indeed the approach is a simplification of the actual phenomena.

1-D/2-D Sketch of the Kiln



Governing Equations

$$\dot{m}_s c_{ps} \frac{dT_s}{dz} = Q_{\text{radiation},g \rightarrow s} + Q_{\text{convection},g \rightarrow s} + Q_{\text{conduction},w \rightarrow s}$$

$$Q_{\text{gas} \rightarrow \text{wall}} + Q_{\text{radiation} \rightarrow \text{wall}} + Q_{\text{solids} \rightarrow \text{wall}} = Q_{\text{shell} \rightarrow \text{ambient}}$$

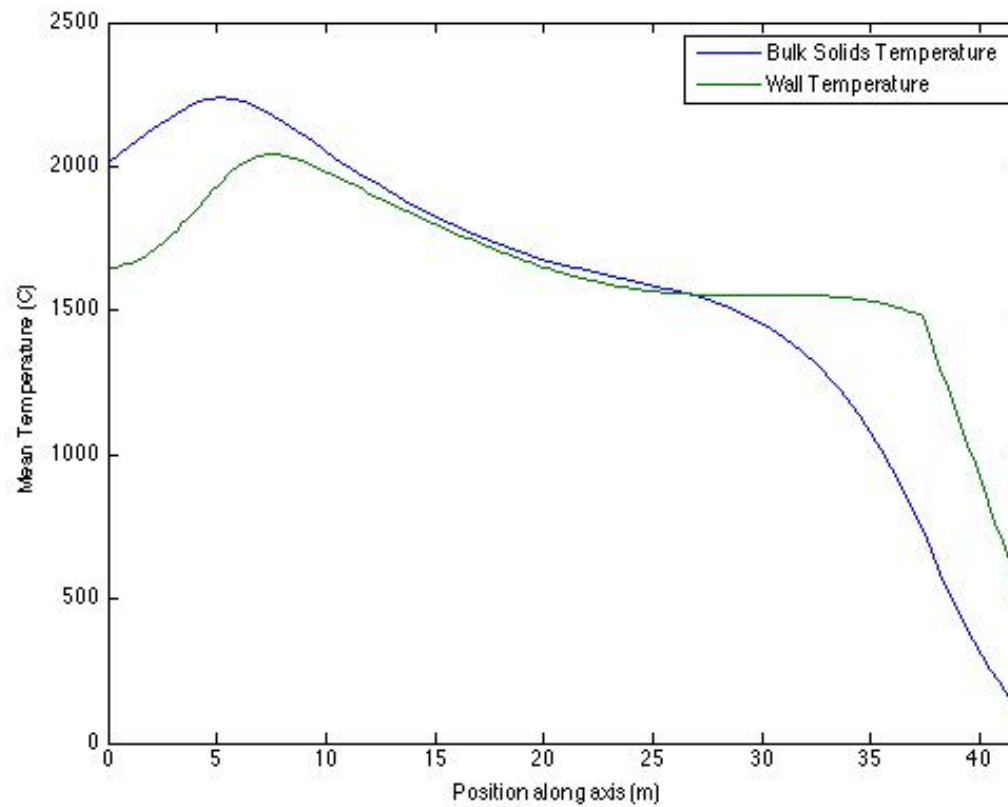
Governing Equations

$$\dot{m}_s c_{ps} \frac{dT_s}{dz} = Q_{\text{radiation},g \rightarrow s} + h_{\text{conv}} A_{g \rightarrow s} (T_g - T_s) + h_{\text{cond}} A_{w \rightarrow s} (T_w - T_s)$$

$$h_{\text{conv}} = 0.4 G_g^{0.62} \quad Nu = \frac{h_{\text{cond}} R \xi}{k_b}$$

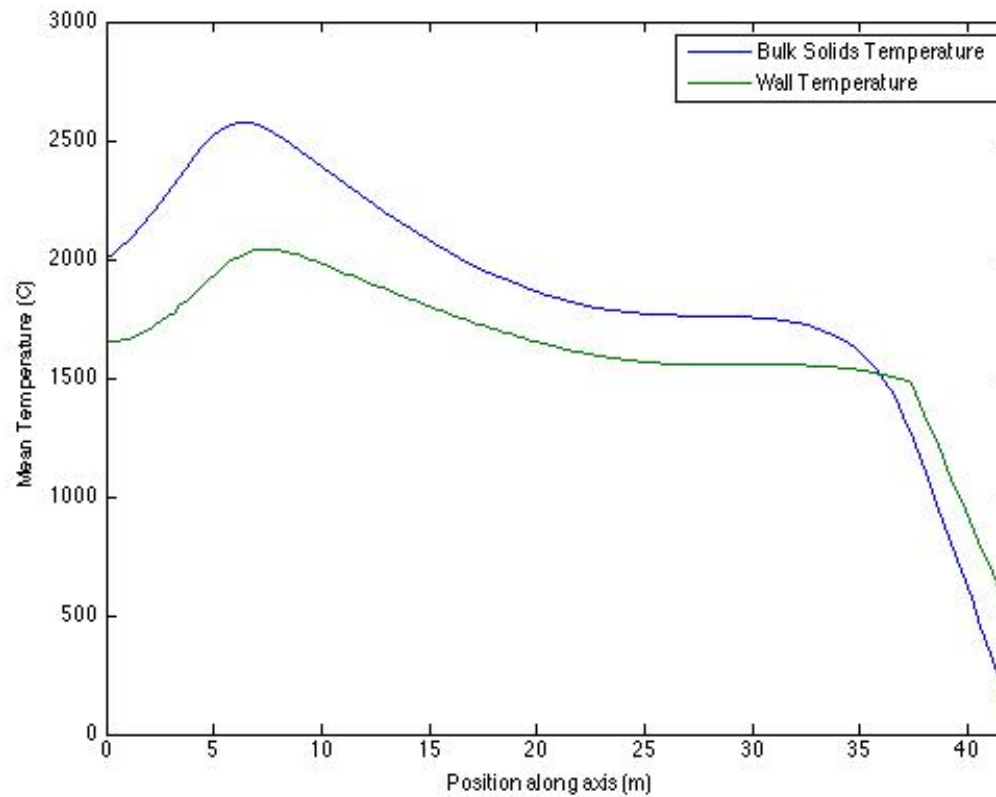
$$Nu = 11.6 Pe^{0.3} \quad Pe = \frac{R^2 \xi \omega}{\alpha_b}$$

Preliminary Results



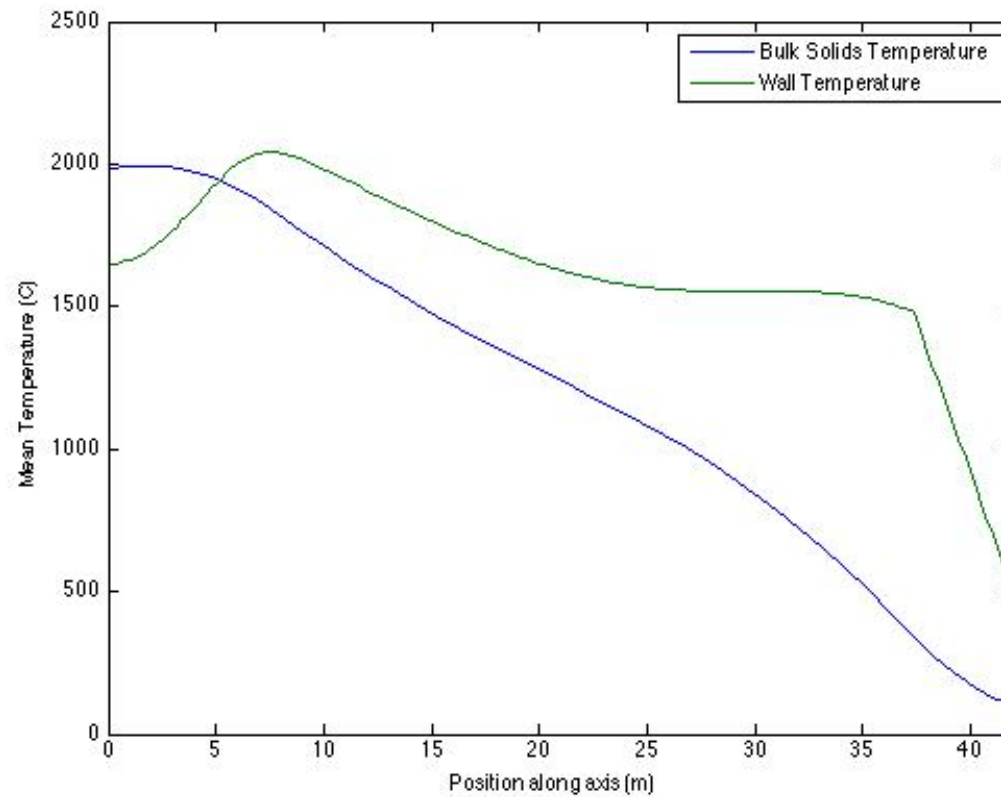
Base Case: 4500 kg/h, 500 Nm³/h, 100 C

Preliminary Results



High gas velocity

Preliminary Results



Higher Kiln loading/Lower Gas Velocity



Further work on 1-D model

- Calibration with data calculated by M. Pisaroni
- Selection of convective heat transfer correlation
- Validation with data from the Kiln, thermocouples and discharge end temperatures
- Sensibility analysis on Gas velocity, Mass Flow and Solids initial Temperature.

What comes next?

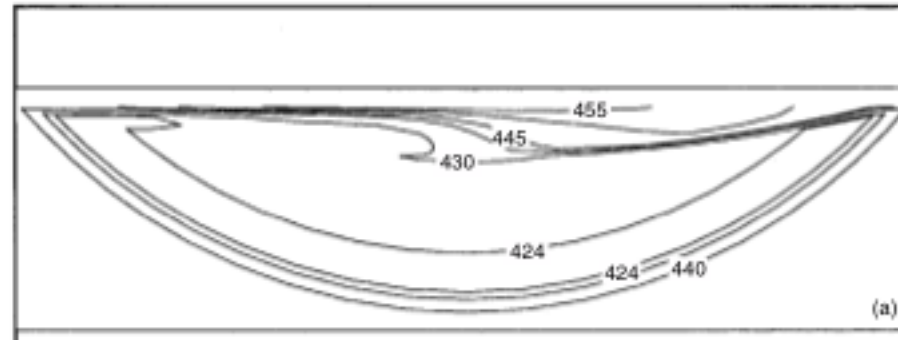
- 1-D Model
 - Calibration and Validation
- Transversal Flow Model (DEM)
 - Calibration and Scale Up to actual kiln size
- PDE Heat Transfer Model
 - Setup, calibration and validation



PDE Heat Transfer Model

- Model described by Boateng,
- Uses Input from a Transversal Flow model which in our case is a DEM simulation,
- Uses same physical correlations as 1-D model and similar governing equations

Sample Output



$$\frac{\partial}{\partial x} \left(k_{\text{eff}} \frac{\partial T}{\partial x} \right) - \rho c_p u_x \frac{\partial T}{\partial x} + \frac{\partial}{\partial y} \left(k_{\text{eff}} \frac{\partial T}{\partial y} \right) - \rho c_p u_y \frac{\partial T}{\partial y} + \dot{m}_b c_{p_b} \frac{dT_{\text{bo}}}{dz} = 0$$

*Images from Boateng



Thank you for your Time!

Questions?